

Gaseous Molecular Sieving Property of a Microporous Hollandite-type Hydrous Manganese Oxide

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A microporous hollandite-type manganese oxide having protons as counter ions (H-Hol) was prepared by hydrothermal reaction and adsorption of various molecules from gas phase was examined. It is found that only H₂O and NH₃ can be adsorbed in the intra-pores; NH₃ is inserted as NH₄⁺ as a result of reacting with lattice protons. Chemisorption of NH₃ is available even under co-existence of water, indicating that H-Hol can be an excellent selective trapper toward odor NH₃.

As one of microporous manganese oxide groups, hollandite-type manganese oxide (H-Hol) has a (2 × 2) tunnel structure whose pore opening can be estimated as 0.46 nm from crystalline data.^{1,2} Although its structural specificity leads to hopeful application as rechargeable batteries²⁻⁵ and as an ion-sieving sorbent towards cations from liquid phase,⁶⁻⁹ its adsorption property toward gaseous molecules has not been sufficiently studied. Recently, we found that NH₃ having an effective diameter of 0.26 nm can be inserted into the tunnel structure of H-Hol from gaseous phase.¹⁰ However, this property was not compared with those of other molecules with pore diameters below 0.46 nm. In this letter, we report the adsorption results using typical adsorbates of nitrogen, oxygen, water, and ammonia, and selective adsorption toward ammonia under co-existence of water, from which the gaseous molecular sieving property of H-Hol will be elucidated.

H-Hol was synthesized by a hydrothermal reaction of an Li₂MnO₃ precursor in a 3 M sulfuric acid solution at 363 K for 48 h.^{10,11} The Li₂MnO₃ precursor was prepared by calcining the mixture of MnOOH and Li₂CO₃ at 1073 K for 48 h. The crystal structure of the prepared H-Hol was confirmed by powder X-ray diffraction (XRD) technique using a Rigaku RINT1200 diffractometer, as having a tetragonal unit cell with size of a = b = 0.981 nm and c = 0.286 nm, similar as that of natural cryptomelane (KMn₈O₁₆).¹² Adsorption isotherms of N₂ and O₂ were measured at 77 K while those of H₂O and NH₃ at 298 K using volumetric methods (Belsorp 18 of Japan Bell Co. and Autosorb-1 of Quanta-Chrom Co.). Before adsorption, samples were pre-evacuated under 1 mPa for 2 h at 573 K for N₂ and O₂ and at 393 K for H₂O and NH₃. After completely obtaining an adsorption isotherm (first run adsorption), a second run adsorption of H₂O or NH₃ was carried out at 298 K after evacuating the sample at the same temperature for 2 h in case of H₂O and for 30 min in case of NH₃. IR absorbance on NH₃ adsorption under atmosphere or co-existence of H₂O was in-situ recorded using a Nicolet NEXUS 470 spectrometer in a resolution of 2 cm⁻¹ and with 32 scans.

Figure 1 shows adsorption isotherms of N₂, O₂, H₂O, and NH₃. All the isotherms are of the shape of typical type IV,^{13,14} which is characteristic of multi-layer adsorption. The NH₃ adsorption amount at the first run is around two or three-fold more than those of the other adsorbates. The second run adsorp-

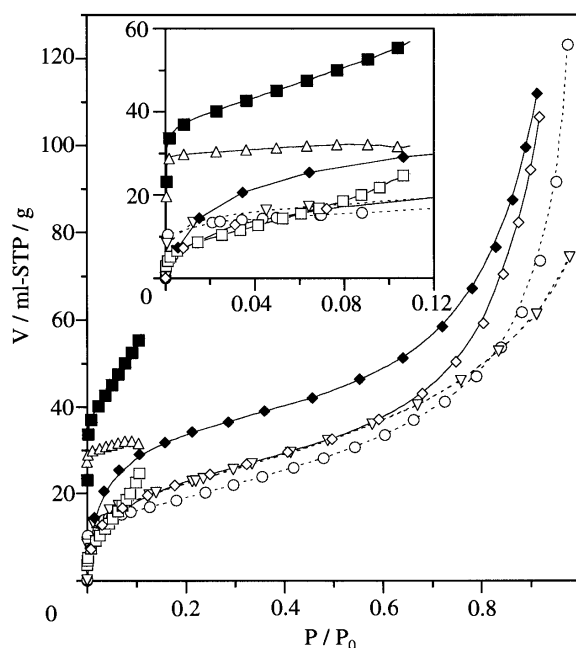


Figure 1. Adsorption isotherms of N₂ (○) and O₂ (▽) at 77 K, NH₃ of the first run (■), the second run (□), and the difference of the first and the second runs (△) at 298 K, H₂O of the first (◆) and the second (◇) runs at 298 K.

tions of H₂O and NH₃ overlap with each other, indicating that their physical adsorptions are exactly the same. Existence of irreversible adsorption (the difference of first and second run adsorption) of H₂O and NH₃ indicates the presence of stronger interaction between protons on H-Hol and the two adsorbates. As the molecular diameter is different from one another among the used adsorbates, the sequence of adsorption could not necessarily reflect whether an adsorbate is inserted or not into the micropores. For this reason, the specific surface areas (S_{BET}) are calculated by Brunauer-Emmett-Teller (BET) method from N₂, O₂, H₂O and NH₃ adsorption isotherms with data on molecular cross-sectional areas recommended by previous contributors (N₂: 0.162 nm², O₂: 0.143 nm², H₂O: 0.125 nm², NH₃: 0.129 nm²).^{13,15,16} The irreversible adsorption areas for NH₃ and H₂O are obtained by the difference between those from the first and second runs. In addition, the total ($S_{\text{t, total}}$), internal ($S_{\text{t, int}}$), and external ($S_{\text{t, ext}}$) surface areas based on N₂ adsorption are calculated by De-Boer's t-plot method using a non-porous alumina's data as a reference.¹⁷ Table 1 shows the values of specific surface areas. From this table, the S_{BET} values from N₂ and O₂ adsorption are much less than those from H₂O and NH₃ adsorption. Since the value of $S_{\text{t, ext}}$ is comparable with that of $S_{\text{t, total}}$, N₂ together with O₂ having a

Table 1. Specific surface area of H-Hol calculated from each gas adsorption

Adsorbate	Molecular Diameter ¹⁹ / nm	Adsorption Temperature / K	S _{BET} / m ² /g	S _{t, total} / m ² /g	S _{t, ext} / m ² /g	S _{t, int} / m ² /g
N ₂	0.364	77	73	68	56	12
O ₂	0.346	77	71			
NH ₃ - 1st run	0.26	298	161			
NH ₃ - 2nd run		298	90			
NH ₃ - irreversible		298	71			
H ₂ O - 1st run	0.265	298	95			
H ₂ O - 2nd run		298	63			
H ₂ O - irreversible		298	32			

similar molecular diameter should mainly be adsorbed onto the external surface of H-Hol irrespective of a greater crystalline pore opening (about 0.46 nm). As the effective pore opening width can be approximated as 0.22 nm after subtracting the contribution of two lattice O²⁻ ionic radius (~ 0.122 nm for three coordination number²⁰) from the crystalline pore opening value (~ 0.46 nm), exclusion of N₂ and O₂ from the micropores can be attributed to the blockade effect of lattice oxygen near the tunnel entrance. On the other hand, H₂O and NH₃ could be inserted into the intra-pores because their surface areas from the first run adsorptions are greater by 1.7 and 2.9 fold, respectively, than S_{t, ext}. Especially, the highest S_{BET} from the first run NH₃ adsorption reveals that NH₃ possibly intrudes into proton barrier inside the tunnel structure.

Figure 2 (a) shows the FT-IR absorbance after NH₃ adsorp-

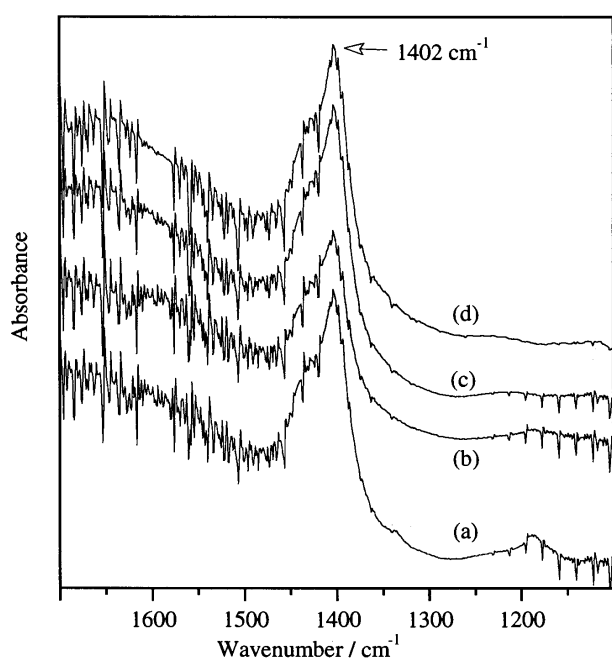


Figure 2. Change in NH₃ adsorption species (NH₄⁺) under co-existence of water.

- (a) 15 min in 27 torr NH₃ at RT after pre-evacuation at 298 K,
 (b) 15 min in 24 torr NH₃ at RT after pre-evacuation at 473 K,
 (c) 15 min in the mixture of 24 torr NH₃ + 3.8 torr H₂O at RT after pre-evacuation at 473 K,
 (d) 2 h exposure to saturated water after evacuation at RT for 15 min following operation (b).

tion. The band at 1402 cm⁻¹ is assigned to an adsorbed NH₄⁺ species,¹⁸ indicating that NH₃ is chemisorbed via a reaction with protons on H-Hol. Another adsorption experiment shows that pre-evacuation at 473 K decreases NH₃ adsorption in agreement with a smaller IR absorbance due to NH₄⁺ species as shown by Figure 2 (b). It is interesting to observe that the presence of water disturbs nothing but slightly enhances NH₃ adsorption after pre-evacuation at 473 K (Figure 2 (c) and (d)). Further researches indicate that there exist two kinds of hydroxyl groups on H-Hol; the weaker one, most possibly existing on the external surface, is lost above 393 K. Weak hydroxyl groups can be recovered under a condition of water exposure, which have relationship with the enhancement in NH₃ adsorption. Thus, the above results show that only water and ammonia can be inserted into the micropores of H-Hol while NH₃ is inserted as NH₄⁺. H-Hol can be an excellent selective trapper toward odor NH₃ molecules.

References and Notes

- R. N. De Guzman, Y. Shen, B. R. Shaw, S. L. Suib, and C. O'Young, *Chem. Mater.*, **5**, 1395 (1993).
- S. Bach, J. P. Pereira-Ramos, and N. Baffier, *Solid State Ionics*, **80**, 151 (1995).
- M. H. Rossouw, D. C. Liles, and M. M. Thackeray, *Mat. Res. Bull.*, **27**, 221, (1992).
- Y. Shao-Hom, S. A. Hackney, C. S. Johnson, and M. M. Thackeray, *J. Electrochem. Soc.*, **145**, 582 (1998).
- T. Ohzuku, M. Kitagawa, K. Sawai, and T. Hirai, *J. Electrochem. Soc.*, **138**, 360 (1991).
- M. Tsuji and M. Abe, *Bull. Chem. Soc. Jpn.*, **58**, 1109 (1985).
- M. Tsuji and M. Abe, *Solvent Ext. Ion Exch.*, **2**, 253 (1984).
- Y. Tanaka, *J. Porous Mat.*, **2**, 135 (1995).
- Q. Feng, H. Kanoh, Y. Miyai, and K. Ooi, *Chem. Mater.*, **7**, 148 (1995).
- S. Tezuka, Z.-M. Wang, K. Ooi, and H. Kanoh, "Proceeding of the 2nd Pacific Basin Conf. On Adsorp. Sci. & Technol.," Brisbane, Australia, in press.
- M. H. Rossouw, D. C. Liles, and M. M. Thackeray, *Mater. Res. Bull.*, **27**, 221 (1992).
- JCPDS-ICDD Powder Diffraction File No. 20-908.
- S. J. Gregg and K. S. W. Sing, "Adsorption, Surface Area and Porosity," 2nd ed, Academic Press, London (1982).
- K. S. W. Sing, D. H. Everett, R. A. W. Haul, L. Moscou, R. A. Pierotti, J. Rouquerol, and T. Siemieniewska, *Pure Appl. Chem.*, **57**, 603 (1985).
- A. L. McClellan and H. F. Harnsberger, *J. Colloid Interface Sci.*, **23**, 577 (1967).
- D. M. Young and A. D. Crowell, "The Physical Adsorption of Gases," Butterworth & Co., (Publishers) Ltd., London (1962).
- B. C. Lippens and J. H. de Boer, *J. Catal.*, **4**, 319 (1965).
- A. A. Tsyganenko, D. V. Pozdnyakov, and V. N. Filimonov, *J. Mol. Struct.*, **29**, 299 (1975).
- D. W. Breck, "Zeolite Molecular Sieves - Structure, Chemistry, and Use," Wiley-Interscience, New York (1974).
- Kagakubinran, 4th ed, Maruzen, Tokyo (1993), vol 2, p. 726.